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APPLICATION NO.	FILING DATE	FIRST NAMED INVENTOR	ATTORNEY DOCKET NO.	CONFIRMATION NO.
10/719,504	11/21/2003	Terry R. Galloway	3178-12	3010
7590 10/06/2005 .		EXAMINER		
Coudert Brothers LLP			LEWIS, BEN	
One Market				
Spear Street Tower, Suite 2100			ART UNIT	PAPER NUMBER
San Francisco, CA 94105			1745	

DATE MAILED: 10/06/2005

Please find below and/or attached an Office communication concerning this application or proceeding.

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	Applicati	on No.	Applicant(s)	
, 	10/719,5	10/719,504	GALLOWAY, TERRY R.	
Office Action Summary	Examine	r	Art Unit	
:	Ben Lewi		1745	
The MAILING DATE of this communi Period for Reply	ication appears on th	e cover sheet with	the correspondence address	
A SHORTENED STATUTORY PERIOD FOWHICHEVER IS LONGER, FROM THE Market SIX (6) MONTHS from the mailing date of this common If NO period for reply is specified above, the maximum states are to reply within the set or extended period for reply Any reply received by the Office later than three months at earned patent term adjustment. See 37 CFR 1.704(b).	AILING DATE OF TI of 37 CFR 1.136(a). In no ev unication. Itutory period will apply and w will, by statute, cause the app	HIS COMMUNICA rent, however, may a rep rill expire SIX (6) MONTH plication to become ABA	ATION. lly be timely filed HS from the mailing date of this communication. NDONED (35 U.S.C. § 133).	
Status			•	
1) Responsive to communication(s) file	d on			
1) Responsive to communication(s) file 2a) This action is FINAL .	d 0⊓ 2b)⊠ This action is r	on final		
3) Since this application is in condition if	·—		re prosecution as to the marite is	
closed in accordance with the practic	•		• •	
·	oo anaor 2x parto at	3dy10, 1000 O.D.	11, 400 0.0. 210.	
Disposition of Claims				
4)⊠ Claim(s) <u>1-31</u> is/are pending in the a	pplication.			
4a) Of the above claim(s) <u>17-31</u> is/are	e withdrawn from co	nsideration.		
5) Claim(s) is/are allowed.			·	
6)⊠ Claim(s) <u>1-16</u> is/are rejected.				
7) Claim(s) is/are objected to.				
8) Claim(s) are subject to restric	tion and/or election r	equirement.		
Application Papers				
9) The specification is objected to by the	e Examiner.			
10)⊠ The drawing(s) filed on <u>21 November</u>	<u>· 2003</u> is/are: a)⊠ a	ccepted or b)	objected to by the Examiner.	
Applicant may not request that any object	ction to the drawing(s) I	be held in abeyanc	e. See 37 CFR 1.85(a).	
Replacement drawing sheet(s) including				
11) The oath or declaration is objected to	by the Examiner. N	ote the attached	Office Action or form PTO-152.	
anionity, under 25 H C C S 440				
Priority under 35 U.S.C. § 119			·	
12) ☐ Acknowledgment is made of a claim t	for foreign priority un	der 35 U.S.C. § 1	119(a)-(d) or (f).	
a) ☐ All b) ☐ Some * c) ☐ None of:				
1. Certified copies of the priority				
2. Certified copies of the priority			· · · · · · · · · · · · · · · · · · ·	
3. Copies of the certified copies of	•		eceived in this National Stage	
application from the Internation	•	, .,		
* See the attached detailed Office action	n for a list of the cert	mea copies not re	eceivea.	
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: .ttachment(s)				
) X Notice of References Cited (PTO-892)		4) Interview Su	mmary (PTO-413)	
2) Notice of Draftsperson's Patent Drawing Review (P		Paper No(s)/	Mail Date	
 Information Disclosure Statement(s) (PTO-1449 or Paper No(s)/Mail Date 4/5/04. 	PTO/SB/08)	5) Notice of Info	ormal Patent Application (PTO-152)	
Patent and Trademark Office		-//	······································	
OL-326 (Rev. 7-05)	Office Action Summa	ary	Part of Paper No./Mail Date 20051003	

DETAILED ACTION

1. Applicants election without traverse of Group I, claims 1-16, in Paper filed July 29th 2005 is acknowledged. Claims 17-31 are withdrawn from consideration.

Claim Rejections - 35 USC § 103

- 2. The following is a quotation of 35 U.S.C. 103(a) which forms the basis for all obviousness rejections set forth in this Office action:
 - (a) A patent may not be obtained though the invention is not identically disclosed or described as set forth in section 102 of this title, if the differences between the subject matter sought to be patented and the prior art are such that the subject matter as a whole would have been obvious at the time the invention was made to a person having ordinary skill in the art to which said subject matter pertains. Patentability shall not be negatived by the manner in which the invention was made.
- 3. Claims 1 is rejected under 35 U.S.C. 103(a) as being unpatentable over Galloway (U.S. Patent No. 6,187,465 B1) in view of Webster, Jr. et al. (U.S. Patent No. 6,086,722)

With respect to claims 1,3 and 7, Galloway discloses a process and system for converting carbonaceous feedstocks into energy without greenhouse gas emissions wherein the process and system of the invention converts carbonaceous feedstock from fossil fuels and other combustible materials into energy without the production of unwanted greenhouse emissions. The present process comprises the following steps:

(a) converting a carbonaceous feedstock and a greenhouse gas stream in a gasification unit to synthesis gas comprising carbon monoxide and hydrogen;

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(b) electrochemically oxidizing at least a portion of the synthesis gas from the gasification unit in a first half-cell of a fuel cell to produce a first half-cell exit gas comprising carbon dioxide and water;

- (c) recovering the carbon dioxide from the first half-cell exit gas to serve as at least a portion of the greenhouse gas stream in step (a); and
- (d) electrochemically reducing an oxygen-containing gas in a second half-cell of the fuel cell completing the circuit and resulting in the production of electrical energy (Col 2 lines 5-25).

Galloway does not specifically mention that the gasification unit is a non catalytic high temperature, gas phase reactor operating at conditions to achieve a gas exit temperature from at least 700°C to about 1600°C. However, Webster, Jr. et al disclose a process for minimizing evaporator scaling during recovery of liquids and solids from the aqueous effluent discharged during a partial oxidation gasification wherein the partial oxidation reaction is preferably carried out in a free-flow, unpacked non-catalytic gas generator, or gasifier at a temperature within the range of about 700°C to about 2000°C, preferably about 1200°C to about 1500°C (Col 3 lines 9-22). Therefore it would have been obvious to one of ordinary skill in the art to incorporate the non-catalytic gasifier of Webster, Jr. et al into the fuel cell system of Galloway because Webster, Jr. et al teach that under these conditions, about 98% to 99.9% of the hydrocarbonaceous feedstock can be converted to a synthesis gas containing carbon monoxide and hydrogen, also referred to as synthesis gas or syngas. Carbon dioxide and water are

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also formed in small amounts. The hydrocarbonaceous feedstock can be petroleum coke, coal, waste plastic material, sewage, or a suitable combination (Col 3 lines 9-22).

With respect to claim 2, Galloway teach that the present process comprises the following step:

(a) converting a carbonaceous feedstock and a greenhouse gas stream in a gasification unit to synthesis gas comprising carbon monoxide and hydrogen (Col 2 lines 5-25).

With respect to claims 4 and 5, Galloway teach that the process can be used in an electric power producing plant using fossil fuels such as carbonaceous feedstocks including coal, hydrocarbon oil, natural gas, oil shale, and petroleum coke as well as in petroleum refinery and a petrochemical plants (Col 3 lines 35-44).

With respect to claims 8, 10 and 11, Galloway teach that by means of the present process and system, the carbon dioxide in the fuel cell is easily kept separate from the air side and any nitrogen. This carbon dioxide can be recycled back to the gasifier in nearly pure form. Likewise water in pure form can be recycled as well in different amounts under gasifier control system requirements to maintain the ideal hydrogen to carbon monoxide ratio of in the range of about 1.75 to about 2.25. This helps maintain a high hydrogen content in the gasifier so that the gasifier-produced syngas can be used downstream in a chemical reactor such as a Fischer-Tropsch reaction system for

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the production of a variety of useful chemicals ranging from methanol to paraffin waxes (Col 3 lines 9-28).

With respect to claim 9, Galloway teach that the oxidized syngas, consisting essentially of hydrogen and carbon monoxide, leaves anode 42 of fuel cell 26 mostly as water vapor and carbon dioxide. This stream of oxidized syngas passes via line 48 into air-cooled condenser 50, where the water vapor is condensed into liquid water and is removed from the condenser bottoms via line 52 for reuse (Col 4 lines 56-67).

With respect to claim 12, Galloway teach that the process of claim 8 wherein the amount of greenhouse gas stream is adjusted in step (a) so that the combined carbonaceous feedstock and greenhouse gas stream to said gasification unit has a hydrogen to carbon monoxide ratio in the range of about 1.75 to about 2.25 (See Galloway Claim 12).

With respect to claim 13, Galloway teach that the process of claim 1 wherein the oxygen-containing gas in step (d) is air and the nitrogen that remains after the electrical reduction is exited into the atmosphere (See Galloway Claim 13).

With respect to claim 14, Galloway teach that the process of claim 1 wherein said first half-cell of said fuel cell contains an electrolyte surrounding a porous catalytic anode electrode (See Galloway Claim 14).

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With respect to claim 15, Galloway teach that the process of claim 14 wherein said second half-cell of said fuel cell contains an air electrolyte surrounding a catalytic cathode electrode (See Galloway Claim 15).

With respect to claim 16, Galloway teach that the process of claim 15 wherein said first and second half-cells of said fuel cell are separated by an ionically conducting membrane that will not allow passage of components from the respective half-cells (See Galloway Claim 16)

Any inquiry concerning this communication or earlier communications from the examiner should be directed to Ben Lewis whose telephone number is 571-272-6481. The examiner can normally be reached on 8:30am - 5:30pm.

If attempts to reach the examiner by telephone are unsuccessful, the examiner's supervisor, Patrick Ryan can be reached on 571-272-1292. The fax phone number for the organization where this application or proceeding is assigned is 571-273-8300.

Information regarding the status of an application may be obtained from the Patent Application Information Retrieval (PAIR) system. Status information for published applications may be obtained from either Private PAIR or Public PAIR. Status information for unpublished applications is available through Private PAIR only. For more information about the PAIR system, see http://pair-direct.uspto.gov. Should you have questions on access to the Private PAIR system, contact the Electronic Business Center (EBC) at 866-217-9197 (toll-free).

Ben Lewis

Patent examiner
Art Unit 1745

DAH-WEIYUAN PRIMARY EXAMINER